

# Possibilities of water-lithium bromide absorption power cycles for low temperature, low power and combined power and cooling systems

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#### **OUTLINE**

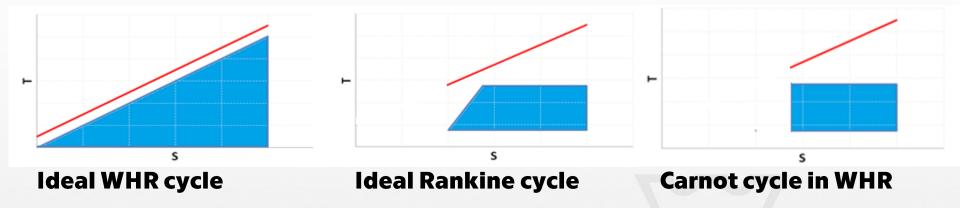
- INTRODUCTION
- CONFIGURATIONS AND MODEL DESCRIPTION
- RESULTS
- CONCLUSION AND FUTURE WORK



#### INTRODUCTION

#### - ISSUES IN LOW TEMPERATURE WASTE HEAT RECOVERY

- Large irreversibility in heat exchangers
- low utilization of the heat source



#### Standard / typical solutions = ORC

- Industrial standard, robust, reliable
- Low heat of vaporization
- Still limited negative effect growing with decreasing heat source temperature
- Result is still very low efficiency, hardly economical application



#### INTRODUCTION

- WASTE HEAT RECOVERY TECHNOLOGIES

#### **SOLUTIONS TO REDUCE IRREVERSIBILITY**

#### Current

Lower latent heat compared to specific heat (ORC cycles)

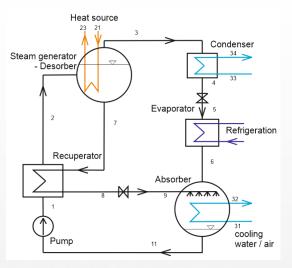
In research or only limited commercialization

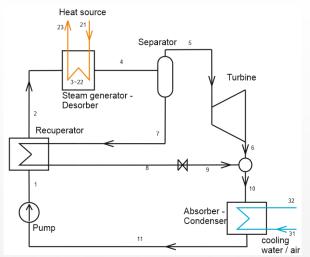
- Variable boiling point
  - use of (zeotropic) mixture as working fluid –temperature match of hot and cold fluid due to temperature glide
- Supercritical state of working fluid
  - no boiling point, specific fluid for specific temperature
- Cascading of multiple cycles, multiple pressure systems
- Trilateral cycle with expansion from saturated liquid

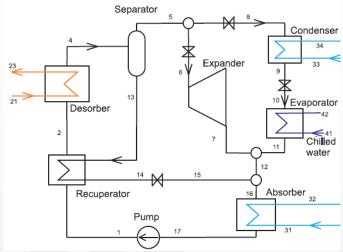


#### INTRODUCTION

- ABSORPTION POWER CYCLE (APC)





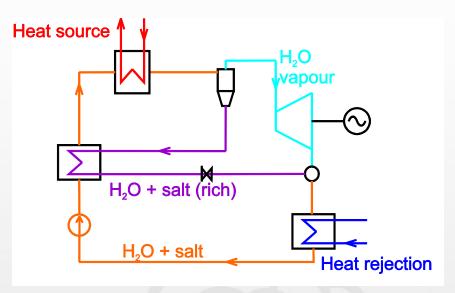


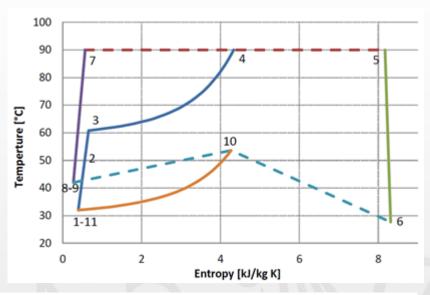
- Working fluids enabling temperature glide of boiling point
- Range of possible working fluids
  - Cooling cycles LiBr H<sub>2</sub>O, H<sub>2</sub>O-NH<sub>3</sub> (commercial), other salts, ionic liquids refrigerants mixtures (mostly only research work)
  - Power cycles previous work limited to NH<sub>3</sub>-H<sub>2</sub>O, only few theoretical works about different working fluids, but their range should be same or larger than for cooling, not so limited by freezing problems
  - Possibility of combining into a single power & cooling system

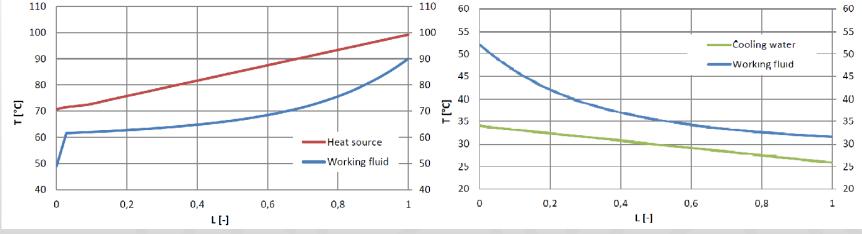


# INTRODUCTION APC technology operation

#### **APC**









# INTRODUCTION APC technology features

- Once through counterflow HXs
  - high exergy efficiency
- Cyclone separator of liquid and vapour
- Whole cycle under vacuum conditions
  - Similarly to absorption cooling
- Vapour free of LiBr and after separation is superheated
- Low pressure allows high efficiency turbine (but bulky)
- Working fluid handling mostly known from chillers

#### **Potential issues**

- Vacuum in whole working fluid area
- Corrosion from the solution
- Large temperature glide in HXs not proven



### CASE SCENARIOS, MODELS DESCRIPTION - GENERAL DESCRIPTION

#### **Case scenarios**

- Small scale WHR
- Low temperature geothermal
- Integration with low temperature solar thermal collector
- Bottoming of cascaded cycles
- Combined cooling and power cycle
- Analysed potential of LiBr APC for each case
- Compared to ORC with R245fa used as a benchmark (simple and for solar also recuperated)

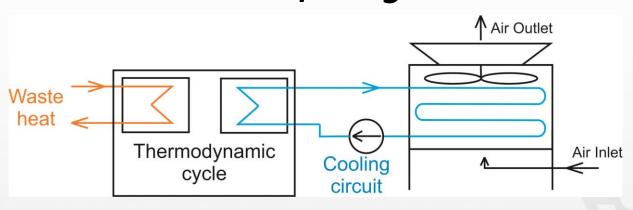
#### **Models**

- Based on mass and energy balance
- Heat transfer defined by selected pinch points
- Included effect of heat rejection parasitic load (dry cooler circuit or air cooled condenser, coolant pressure drop)
- Boundary conditions
  - See the manuscript
- Calculated in Engineering Equation Solver
- Each cycle model optimized for maximal power production



#### **CASES – Waste Heat Recovery**

#### Heat source: 100°C, 10 kg/s hot air



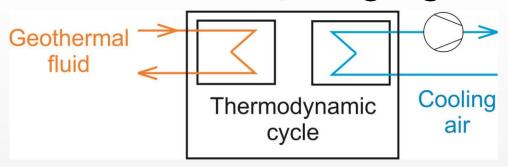
(ORC only nonregenerative as it hasn't thermodynamic benefit)

	$W_c$ [kW]	$W_{net}$ [kW]	$\eta_c \ [\%]$	$\eta_{WHR}$ [%]	$T_{WH~out}$ [°C]	p <sub>c,high</sub> [kPa]	p <sub>c,low</sub> [kPa]
ORC APC	9.58 13.43	5.36 9.78	5.43 5.51	0.63 1.29	85.6 75.9	541 6.7	252 1.7
	<i>m<sub>cw</sub></i> [kg/s]	m <sub>ca</sub> [kg/s]	<i>UA<sub>ev</sub></i> [kW/K		A <sub>cond/abs</sub> [kW/K]	UA <sub>rec</sub> [kW/K]	UA <sub>DC</sub> [kW/K]
ORC APC	3.8 3.2	15.4 13.1	6. 11.		18.3 39.8	2.1	16.7 23.0



#### **CASES – Low Temperature Geothermal**

#### Heat source: 70°C, 10 kg/s geothermal water



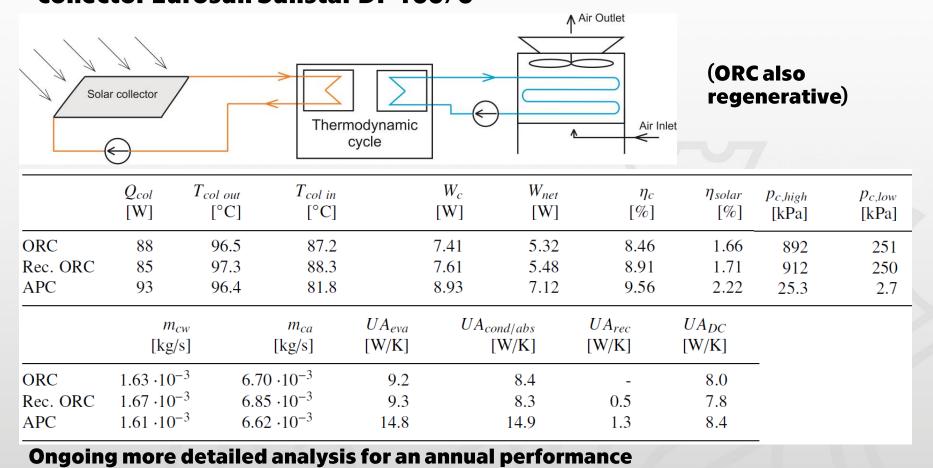
(ORC non-regenerative as it hasn't thermodynamic benefit)

	$W_c$ [kW]	W <sub>net</sub> [kW]	$\eta_c$ [%]	η <sub>WHR</sub> [%]	$T_{geofl}$	uid out [°C]	p <sub>c,high</sub> [kPa]	p <sub>c,low</sub> [kPa]
ORC APC	25.5 36.9	14.2 28.0	4.6 4.47	0.6 1.22		56.7 50.3	382 2.6	199 0.8
	m <sub>ca</sub> [kg/s]	UA <sub>eva</sub> [kW/K]	UA <sub>cond/abs</sub> [kW/K]		UA <sub>rec</sub> [kW/K]			
ORC APC	61.0 50.7	56.3 138.5	38.7 74.5		- 8.9			



#### **CASES – Low Temperature Solar**

# Heat source: solar vacuum collector Case of location ans time – Prague, May ( $G = 321 \text{ W/m}^2$ , $T_{amb} = 14^{\circ}\text{C}$ ), collector Eurosun Sunstar DF 100/6

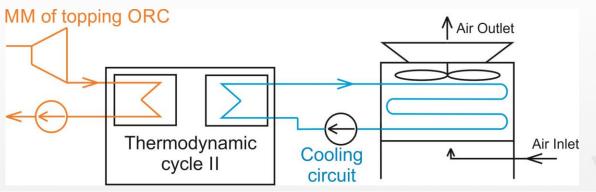




#### **CASES – Bottoming cycle**

#### Heat source: Desuperheating, condensing and subcooling MM

Condensation pressure 74 kPa ~ 90 °C



	$W_c$ [kW]	$W_{net}$ [kW]	$\eta_c \ [\%]$	$\eta_{net} \ [\%]$	<i>P<sub>c,high</sub></i> [kPa]	p <sub>c,low</sub> [kPa]	$m_{cw}$ [kg/s]
ORC	4.15	3.12	8.30	6.23	895	260	0.917
rec. ORC	4.31	3.22	8.62	6.44	895	258	0.965
APC	4.95	3.92	9.89	7.85	51	6	0.179

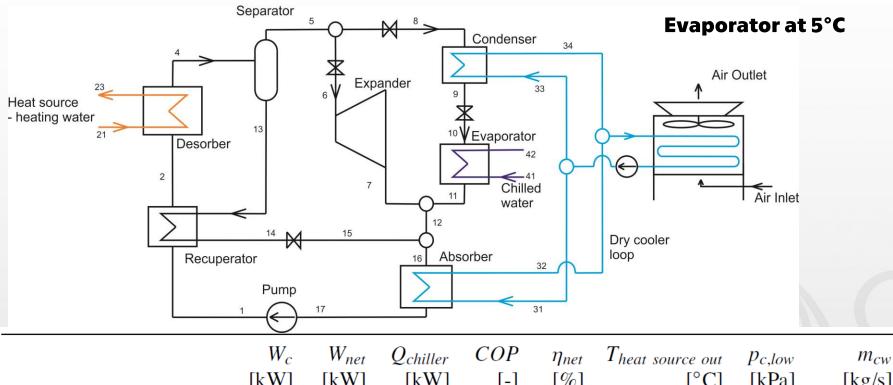
	$m_{ca}$ [kg/s]	$UA_{eva}$ [kW/K]	$UA_{cond/abs} \ [\mathrm{kW/K}]$	$UA_{rec}$ [kW/K]	$UA_{DC}$ [kW/K]
ORC	3.765	6.01	4.81	-	4.56
rec. ORC	3.962	6.23	4.88	0.28	4.57
APC	0.907	6.18	6.22	0.02	4.51

	130 -						
٦٥	110 -						
atne	90 -		-/7				/
Temperature [°C]	70 -					nsing MN . R245fa	Λ
	50 -				R245f		
	30 -		10	20	20	40	
w -1 -		0	10	20 Heat tran	30 sfer [kW]	40	50



# **CASES – Combined Power and Cooling Cycle**

#### **Heat source: 80°C, 1 kg/s water (district heating parameters)**



	$W_c$ [kW]	$W_{net}$ [kW]	Q <sub>chiller</sub> [kW]	<i>COP</i> [-]	$\eta_{net} \ [\%]$	$T_{heat\ source\ out}$ [°C]	p <sub>c,low</sub> [kPa]	m <sub>cw</sub> [kg/s]
Cooling only	-0.001	-3.35	37.6	0.83	-	69.1	0.87	3.02
50% cooling, 50% power	1.60	-0.68	18.8	-	-	69.1	0.87	2.05
Power only	3.20	1.99	0	-	4.37	69.1	0.87	1.08
Power only, optim. abs. p	4.49	3.14	0	-	3.37	57.7	3.03	1.17



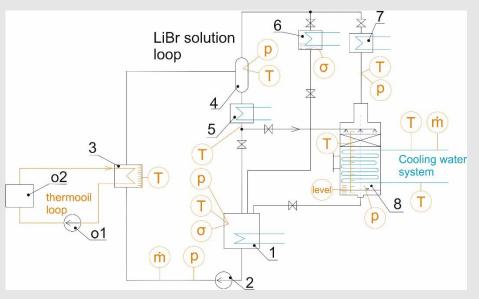
#### **CONCLUSION & FUTURE WORK**

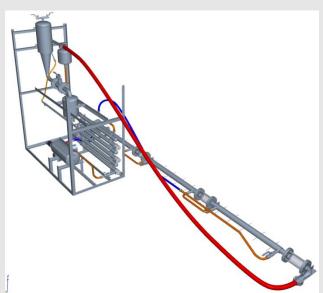
- Low T applications potential of LiBr APC for significant performance increase
- Parasitic load plays a very important role suitable for zeotropic mixture fluids including LiBr APC
- Larger equipment in general
  - Suitable for efficient small turboexpander
  - Larger heat exchangers



#### **CONCLUSION & FUTURE WORK**

- Experimental verification of LiBr APC equipment
  - Investigation of phase change behaviour in counterflow desorber, separator, later absorber





- Demonstration LiBr APC unit
  - Including expander
  - Closer to real operation system but less possibilities for detailed phase change investigation



#### **QUESTIONS?**

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