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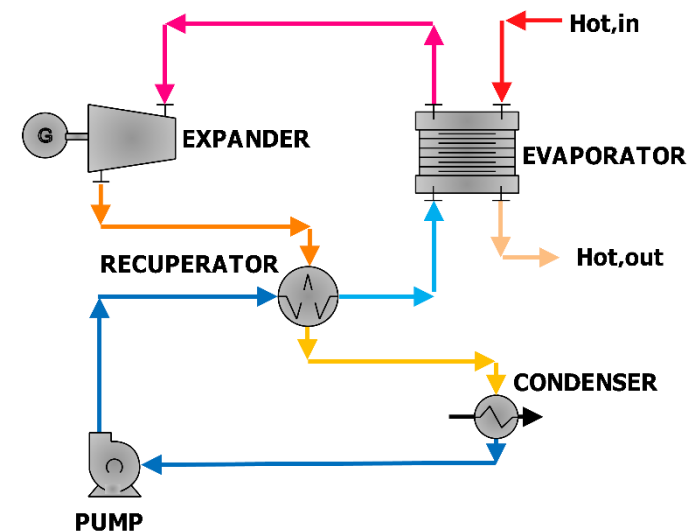
Design and Off-Design Analysis of an ORC Coupled with a Micro-Gas Turbine

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AGENDA

1. Introduction
2. Methodology
3. Case Study
4. Results
5. Conclusions



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INTRODUCTION

- ◇ Energy → Essential → Development → Nations
- ◇ Total Primary Energy Consumption → Based → Non-Renewable Sources
- ◇ Recent Years → Increasing Concern → Energy Systems Environmental Impact
- ◇ New Energy Policies
 - *Renewable Energy Sources*
 - *Energy Efficiency*
 - *Waste Heat Recovery*
- ◇ Waste Heat Recovery → Sources → Medium/Low Temperature Heat Sources → Converted → Electricity

INTRODUCTION

- ◇ Organic Rankine Cycle → Valid Alternative → Conventional Steam Rankine Cycle → Fails
 - *Technical Problems*
 - *Economic Reasons*

- ◇ ORC → Operates → SRC → But → ORC Design
 - *Select → Working Fluid*
 - *Select → Plant Arrangement*

- ◇ Design Point Analysis → Fluid and Plant Configuration → But
 - *Are the Fluid and the Plant Arrangement Able to Guarantee Good Performance During Part-load Conditions??*



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METHODOLOGY

1. Design Point Analysis → ORC-PD tool → Optimisation Code
 - *Fluid Selection*
 - *Plant Configuration Optimisation*
 2. Off-Design Analysis → ASPEN Tools
 - I. Aspen EDR → Heat Exchangers Design*
 - II. Aspen Plus → Plant Off-Design Behaviour*
- ◇ Analyses Results → Fluid, Plant Layout and Control Strategy → Fit → Heat Source Profile

METHODOLOGY: DESIGN POINT OPTIMIZATION

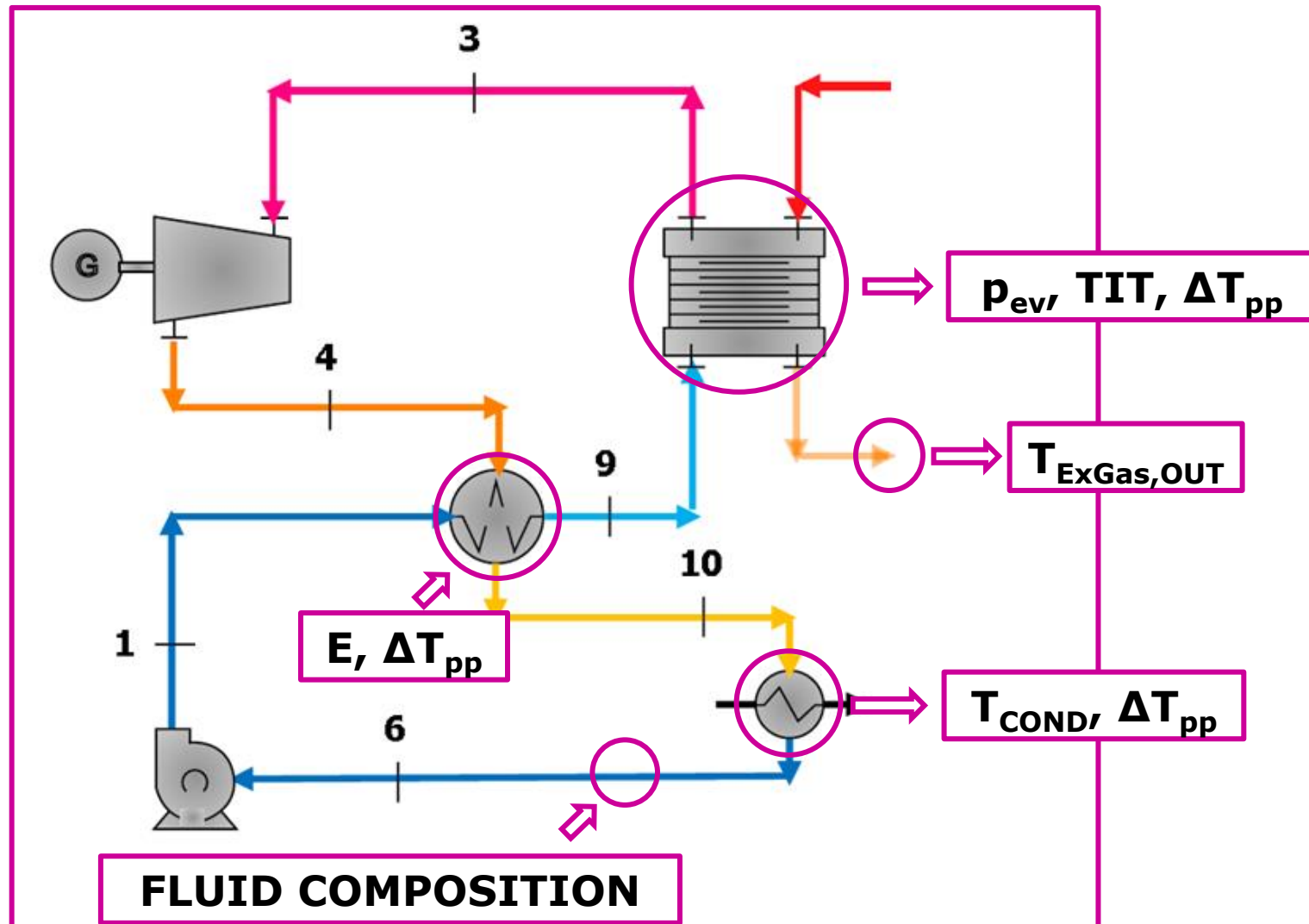
- ◇ ORC-PD tool → MATLAB Environment → CoolProp and REFPROP Databases
 - *Different Heat Sources*
 - *115 Pure Fluids and Their Mixtures*
 - *8 Plant Configurations*
 - *Axial and Radial Turbines Efficiency Charts*
 - *Sub- and Trans-critical Cycles*
- ◇ Possible Objective Functions
 - *Net Electric Power*
 - *Thermal Efficiency*
 - *Exergetic Efficiency*
 - *Profitability Index*
 - *Levelized Cost of Energy*

METHODOLOGY: DESIGN POINT OPTIMIZATION

- ◇ Tool Input Parameters
 - *Heat Sources Medium*
 - *Inlet Temperature and Pressure and Mass Flow of the Heat Source*
 - *Pump Isentropic and Mechanical Efficiency*
 - *Expander Mechanical Efficiency*
 - *Electric Generator Efficiency*
 - *Electric Motor Efficiency*
 - *Sink Type*

METHODOLOGY: DESIGN POINT OPTIMIZATION

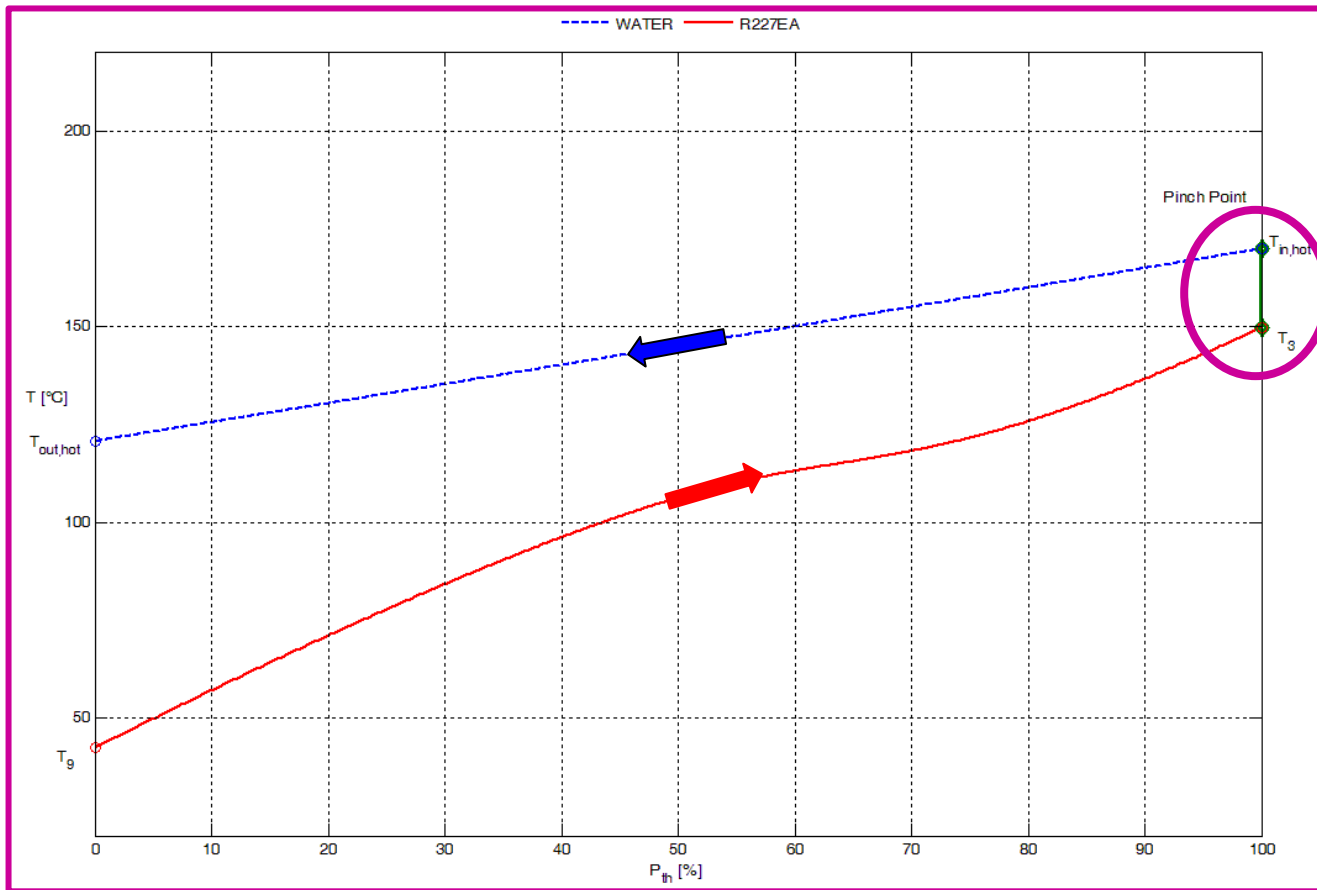
◇ Optimized Variables



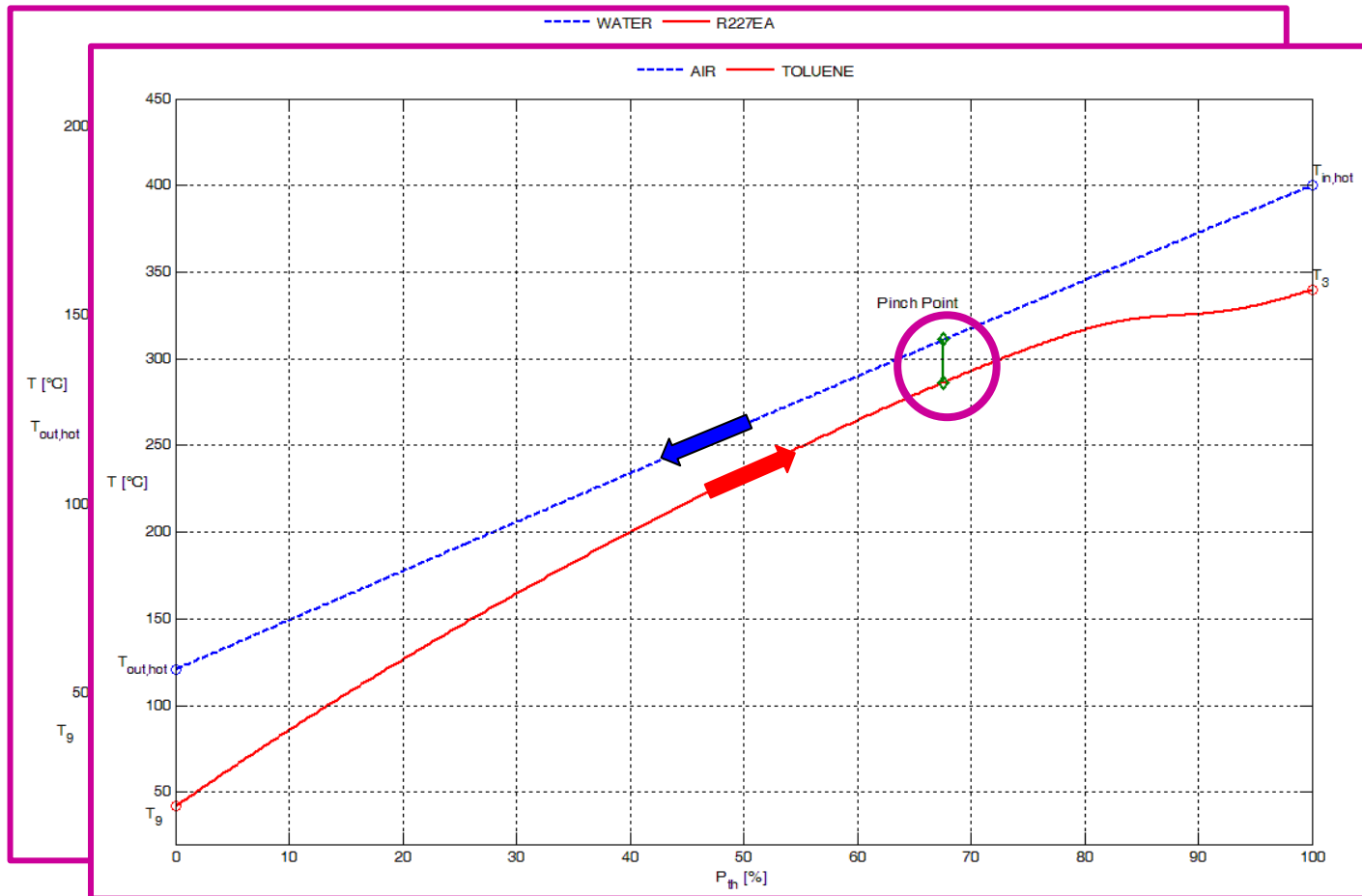
METHODOLOGY: DESIGN POINT OPTIMIZATION

- ◇ Several Checks
 - *Evaporation in the Recuperator*
 - *Liquid at the Turbine Inlet*
 - *Steam Quality at the Turbine Outlet*
 - *Pinch Point Violation in the Heat Exchangers*
- ◇ Each Heat Exchanger → “n” Elements
- ◇ Not Fixed Pinch-Point Position

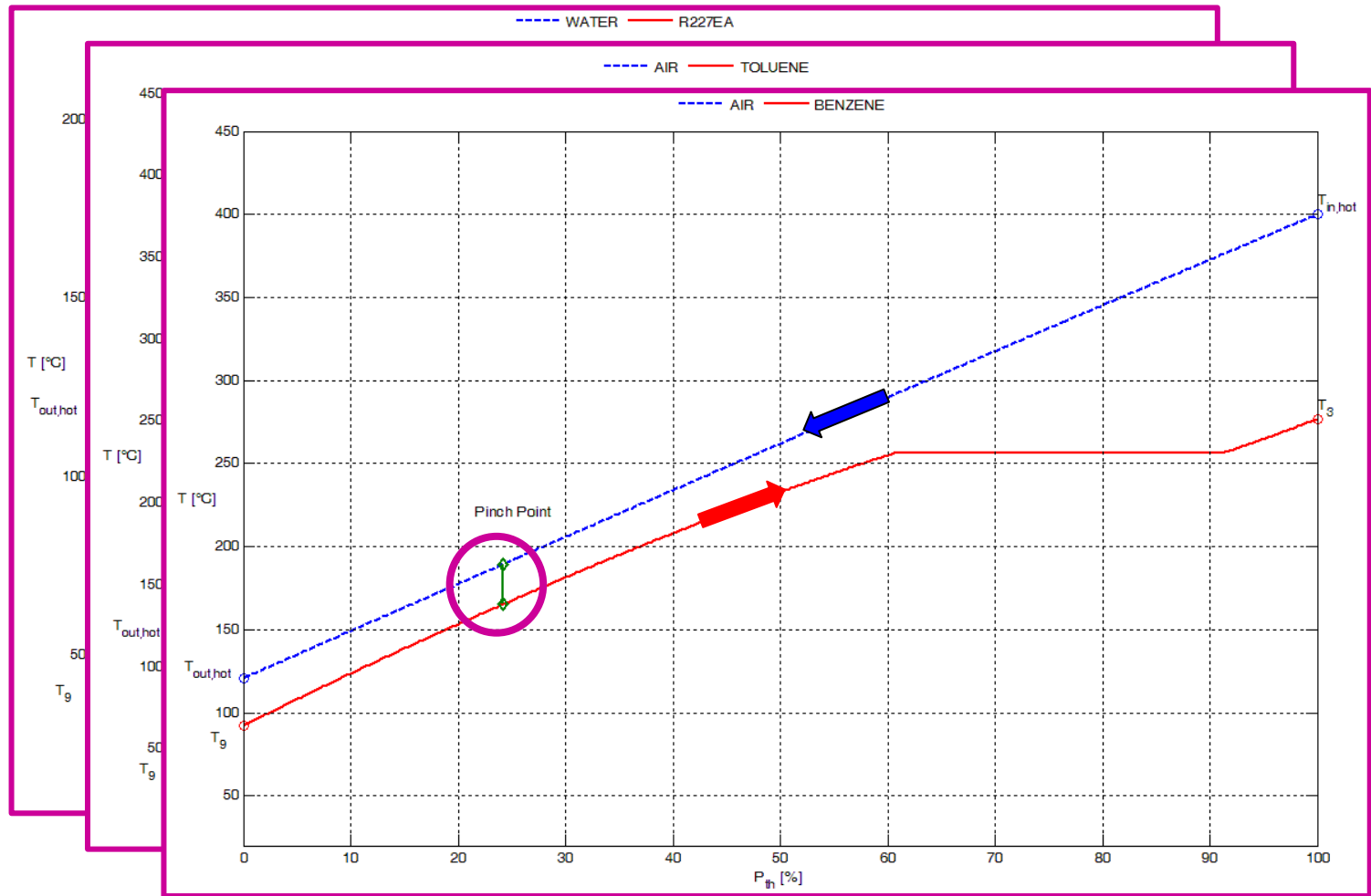
METHODOLOGY: DESIGN POINT OPTIMIZATION



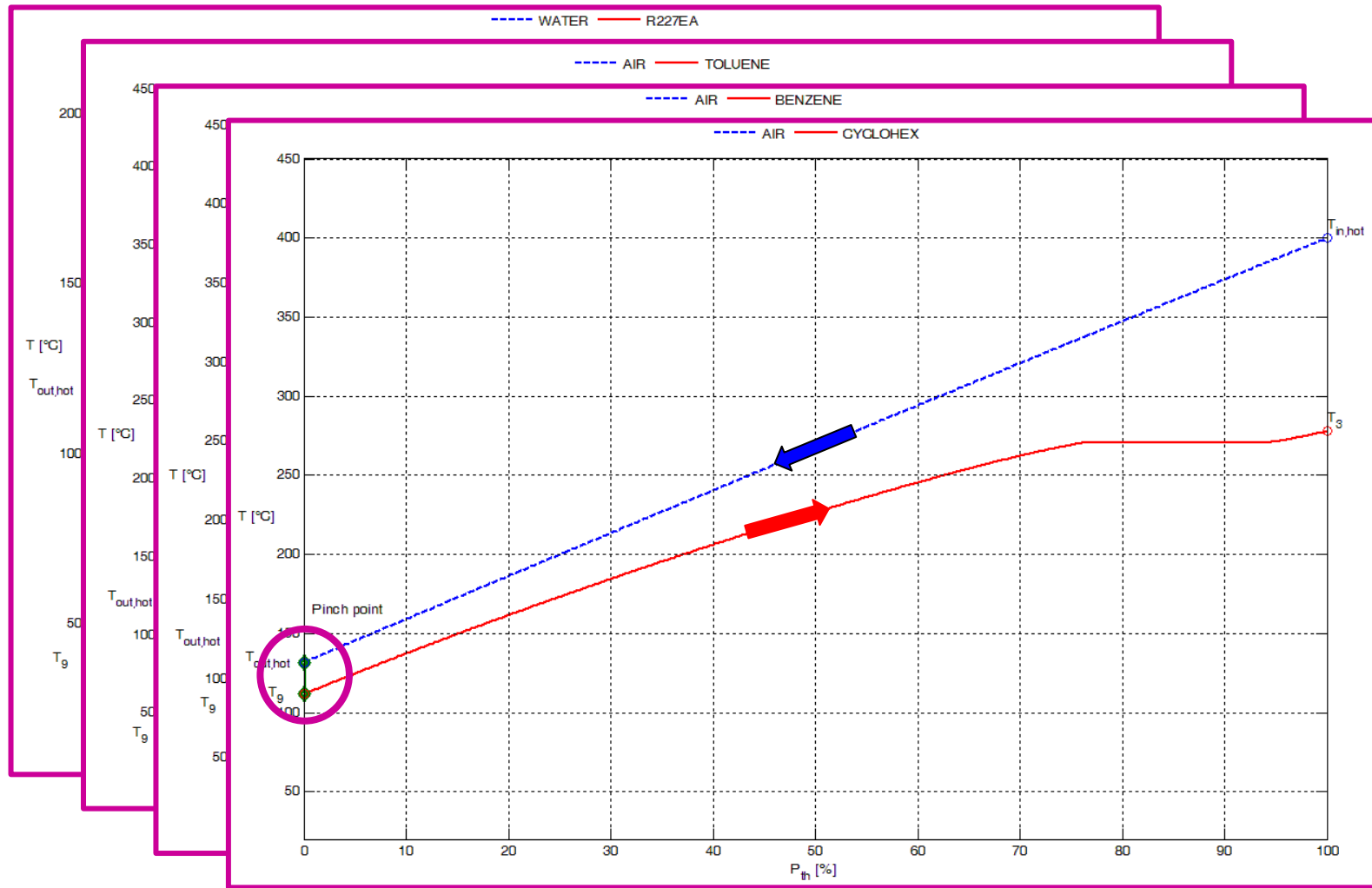
METHODOLOGY: DESIGN POINT OPTIMIZATION



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METHODOLOGY: DESIGN POINT OPTIMIZATION



Improving the Energy Efficiency of a Paint and Cataphoresis Facility with an Organic Rankine Cycle Module
Presenter: Alberto Benato, Department of Industrial Engineering, University of Padova

METHODOLOGY: DESIGN POINT OPTIMIZATION

- ◇ For Each Plant Configuration → ORC-PD tool → Performs → Energy, Exergy and Economic Analysis
- ◇ End → Design Point Optimisation Process
 - *One or More → Good → Working Fluids*
 - *One or More → Good → Plant Layouts*
- ◇ Are They Also Good → Off-Design???

METHODOLOGY: OFF-DESIGN ANALYSIS

- ◇ Aspen Exchanger Design and Rating (EDR) → Heat Exchangers → Detailed → Geometry Design
- ◇ Aspen Plus → ORC Off-Design Model → Predicts → Part-Load Behaviour
 - *Heat Exchangers Geometry*
 - *Turbine → Stodola's Equation*
 - *Pump → Real Centrifugal Pump Efficiency Maps*
 - *Dedicated Control System*



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CASE STUDY

- ◇ Small Manufacturing Industry
 - *Boiler* → *Process Heat & Space Heating* → 250 kW_{th}
 - *Photovoltaic Plant* → 50 kW_{el}
- ◇ Add → 65 kW_{el} m-GT → Exhaust Gases → Electricity Self Production → Non-cogenerative m-GT → Capstone C65
- ◇ Explore → Possibility → Recovers → 65 kW_{el} m-GT Exhaust Gases → Waste Heat Recovery Unit → Organic Rankine Cycle Turbogenerator

CASE STUDY

- ◇ m-GT Main Characteristics
 - *Fluid* → Exhaust Gases
 - *Exhaust Temperature* → 309 °C
 - *Exhaust Mass Flow* → 0.49 kg/s

- ◇ Goal of the Analysis
 - *Best Working Fluid* → *Pure Fluids or Mixtures*
 - *Best Configuration* → *Simple or Recuperative*
 - *Objective Function* → *Maximization of the Net Electric Power*
 - *Design + Off-Design* → *Approach*

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RESULTS: DESIGN POINT ANALYSIS

| Fluid | P_{el} (kW) | E (-) | p_{ev} (bar) | TIT (°C) | $T_{Hot,out}$ (°C) | p_{cond} (bar) | η_{ORC} (%) | NPV (M\$) | IP (-) | SPB (y) |
|-----------------|------------------------------------|-----------------|-------------------------------------|--------------------|---|---------------------------------------|---------------------------------------|---------------------|------------------|-------------------|
| <i>Cyclopen</i> | 12.58 | 0 | 23.2 | 201.8 | 101.8 | 1.85 | 11.5 | 0.033 | 0.168 | 8.9 |
| <i>R141b</i> | 12.42 | 0 | 34.4 | 206.8 | 98.8 | 3.15 | 11.2 | 0.016 | 0.117 | 9.3 |
| <i>Cyclohex</i> | 12.40 | 0 | 10.3 | 183.9 | 102.9 | 0.68 | 11.4 | 0.032 | 0.166 | 8.9 |

- ◇ Cyclopentane → Best Working Fluid in Design
- ◇ Best Configuration → Basic ORC Layout
- ◇ But → Among → Three Fluids → Difference → Produced Power → Really Small

RESULTS: OFF-DESIGN ANALYSIS

- ◇ Off-Design Behaviour → Three Cycles
- ◇ Aspen EDR → Heat Exchangers Design → Geometry → e.g. Cyclopentane

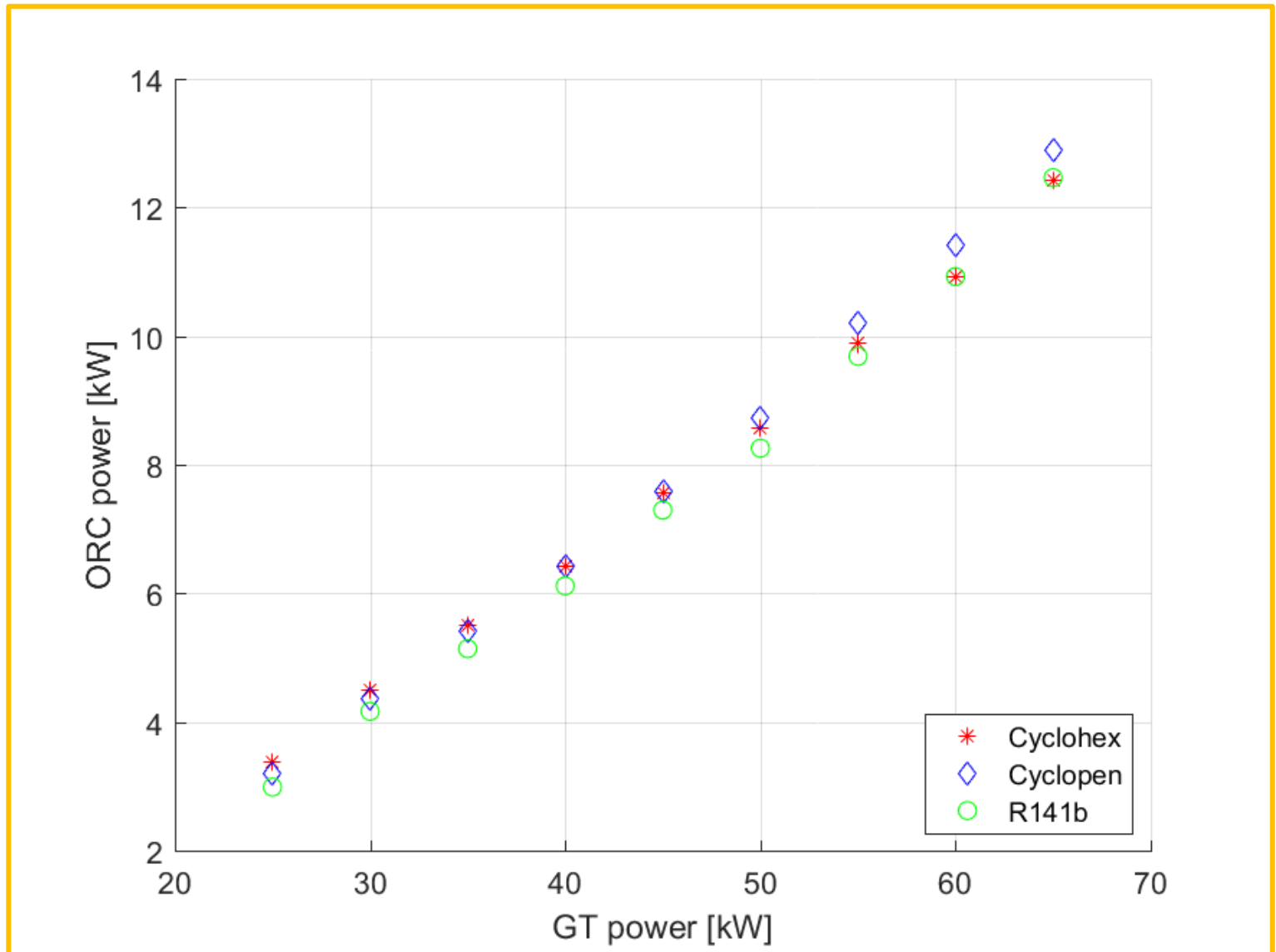
RESULTS: OFF-DESIGN ANALYSIS

| | Evaporator | Condenser |
|--------------------------------------|-------------------|------------------|
| Thermal power (kW) | 106.6 | 94.8 |
| Hot fluid mass flow rate (kg/s) | 0.49 | 0.21 |
| Cold fluid mass flow rate (kg/s) | 0.21 | 2.23 |
| Heat transfer area (m ²) | 35.3 | 4.9 |
| Tube external diameter (mm) | 8 | 10 |
| Tube thickness (mm) | 1 | 1 |
| Tube length (mm) | 2410 | 1830 |
| Shell inner diameter (mm) | 316 | 163 |
| Number of tubes | 594 | 88 |
| Number of passes - shell size | 1 | 1 |
| Number of passes - tube side | 1 | 2 |
| Tube pitch (mm) | 10 | 12.5 |
| Pressure drop - tube side (bar) | 0.03 | 0.12 |
| Pressure drop - shell size (bar) | 0.09 | 0.05 |

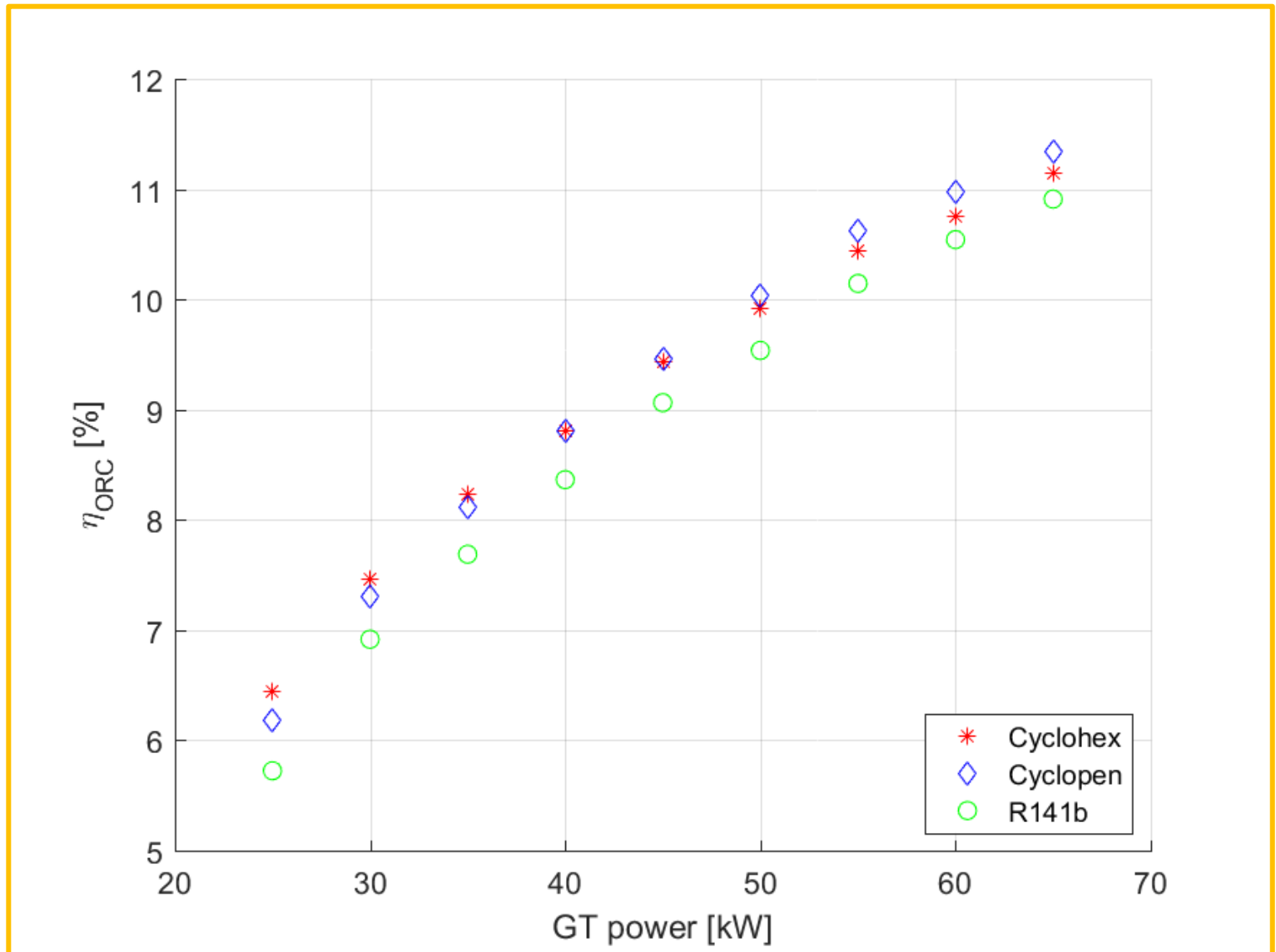
RESULTS: OFF-DESIGN ANALYSIS

- ◇ Off-design Behaviour → Three Working Fluids
- ◇ Aspen EDR → Heat Exchangers Design → Geometry → e.g. Cyclopentane
- ◇ Aspen Plus → Plants Models → Control Strategy → Controlled Variable → Pump Rotational Speed → $TIT = TIT_{\text{design}}$

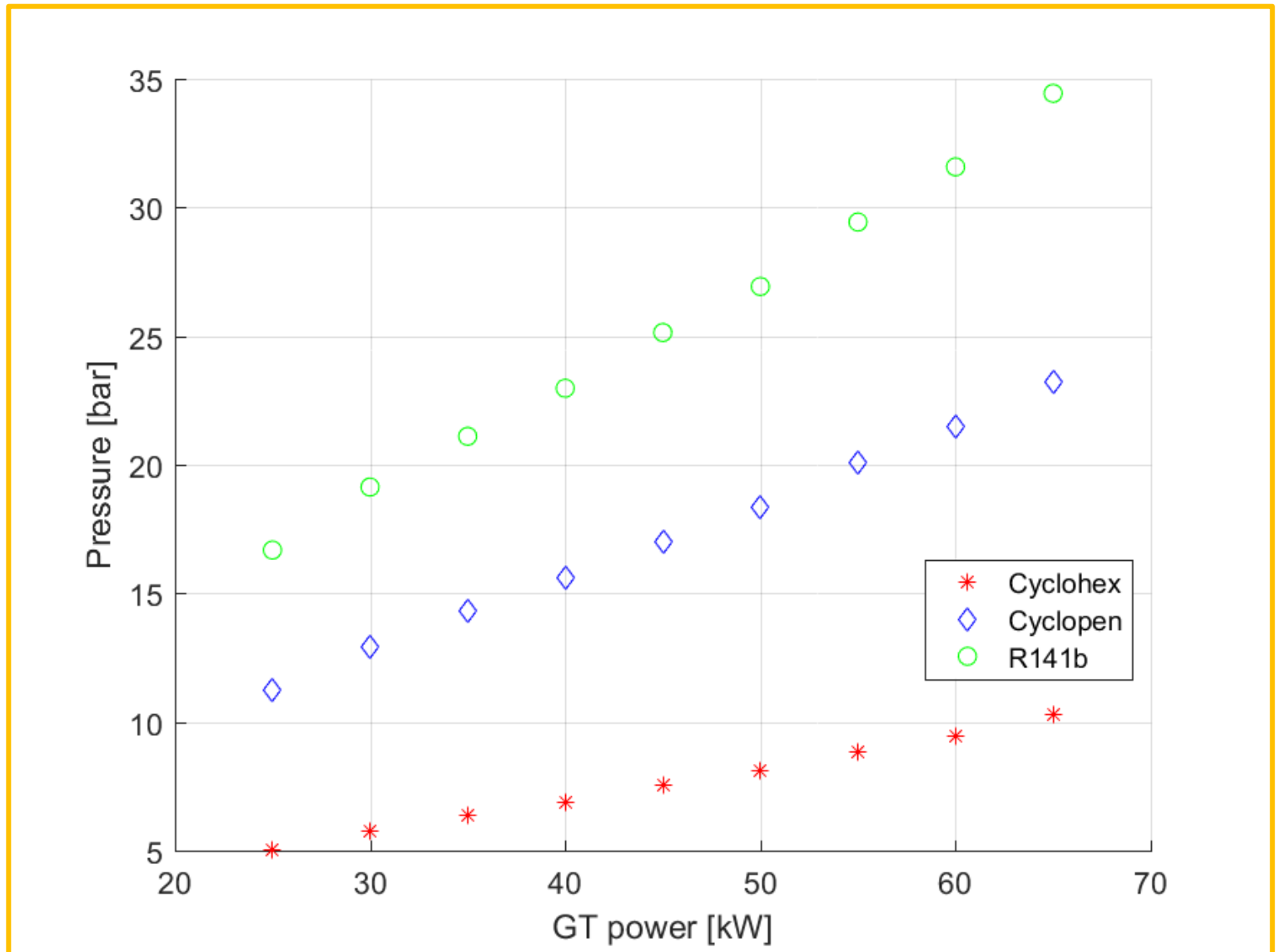
RESULTS: OFF-DESIGN ANALYSIS



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RESULTS: OFF-DESIGN ANALYSIS



RESULTS

- ◇ Cyclopentane → Highest P_{el} → $50 < P_{el,GT} < 65$ kW
- ◇ Cyclohexane & Cyclopentane → Highest P_{el} → $40 < P_{el,GT} < 50$ kW
- ◇ Cyclohexane → Highest P_{el} → $25 < P_{el,GT} < 40$ kW
- ◇ Cyclopentane → Can Be Suggested → Working Fluid → Based → Design and Off-design Analyses

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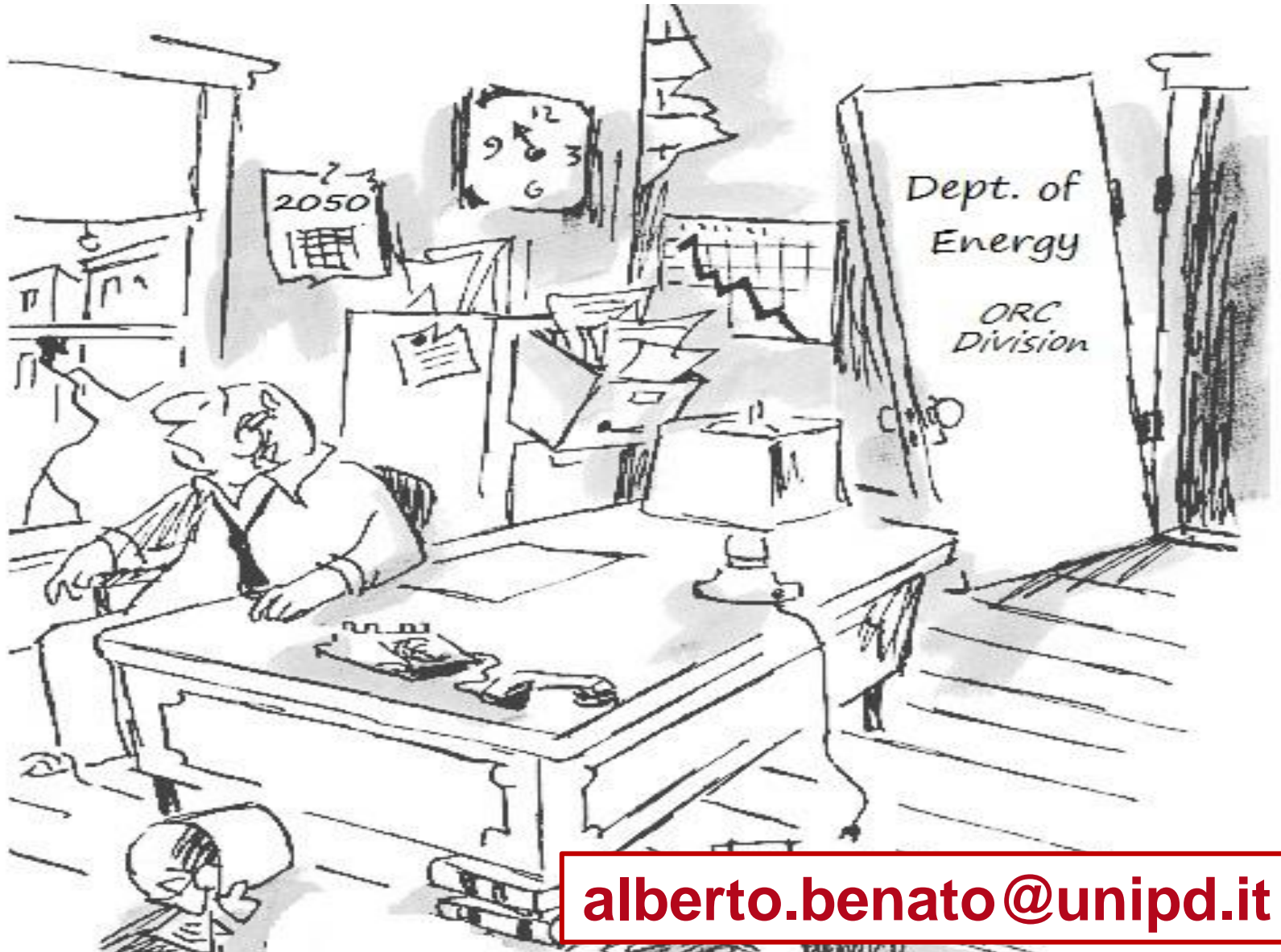
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CONCLUSIONS

- ◇ Goal → Improve → Efficiency → 65 kW_{el} m-GT → Waste Heat Recovery Unit → ORC
- ◇ Methodology → Design point + Off-design Analysis → Select → Best Fluid + Plant Layout → Design Condition
- ◇ ORC-PD tool → Design Point Analysis
- ◇ Aspen EDR+Plus → HXs and Off-design Model
- ◇ Cyclopentane + Basic Layout → Suggested
- ◇ Future Works → Different Control Strategy
- ◇ Future Works → Dynamic Analysis Integration

THANK YOU FOR YOUR ATTENTION!!!!



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